

1 **Modelling dynamic changes in blood flow and volume in the cerebral vasculature**

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12

13 **Abstract**

14 The cerebral microvasculature plays a key role in the transport of blood and the delivery of nutrients
15 to the cells that perform brain function. Although recent advances in experimental imaging
16 techniques mean that its structure and function can be interrogated to very small length scales,
17 allowing individual vessels to be mapped to a fraction of 1 μm , these techniques currently remain
18 confined to animal models. In-vivo human data can only be obtained at a much coarser length scale,
19 of order 1 mm, meaning that mathematical models of the microvasculature play a key role in
20 interpreting flow and metabolism data. However, there are close to 10,000 vessels even within a
21 single voxel of size 1 mm^3 . Given the number of vessels present within a typical voxel and the
22 complexity of the governing equations for flow and volume changes, it is computationally

23 challenging to solve these in full, particularly when considering dynamic changes, such as those
24 found in response to neural activation.

25 We thus consider here the governing equations and some of the simplifications that have been
26 proposed in order more rigorously to justify in what generations of blood vessels these
27 approximations are valid. We show that two approximations (neglecting the advection term and
28 assuming a quasi-steady state solution for blood volume) can be applied throughout the cerebral
29 vasculature and that two further approximations (a simple first order differential relationship
30 between inlet and outlet flows and inlet and outlet pressures, and matching of static pressure at
31 nodes) can be applied in vessels smaller than approximately 1 mm in diameter. We then show how
32 these results can be applied in solving flow fields within cerebral vascular networks providing a
33 simplified yet rigorous approach to solving dynamic flow fields and compare the results to those
34 obtained with alternative approaches. We thus provide a framework to model cerebral blood flow
35 and volume within the cerebral vasculature that can be used, particularly at sub human imaging
36 length scales, to provide greater insight into the behaviour of blood flow and volume in the cerebral
37 vasculature.

38 **1 Introduction**

39 Since 2006 there has been a great deal of interest in models of the cerebral microcirculation. This
40 has been driven by the recent ability to obtain experimental data about microvascular networks,
41 both in humans and in animal models. The former has mainly been based on the collection of post-
42 mortem casts obtained by Duvernoy et al. (1981), and these experimental data have been presented
43 in detail by Cassot et al. (2006), Lauwers et al. (2008) and Lorthois et al. (2011). Casts of animal
44 microvascular networks have also been extracted and the flow in them modelled, see for example
45 Fang et al. (2008), Weber et al. (2008), Reichold et al. (2009), Tsai et al. (2009), Guibert et al. (2010),
46 Blinder et al. (2010), Safaeian et al. (2011), Kasische et al. (2011), Linninger et al. (2013), Gagnon et

47 al. (2015), Gould et al. (2017) and Schmid et al. (2017). Many of the models listed above have also
48 examined the transport of oxygen and the coupling between this and cerebral blood flow.

49 Although there has been a great deal of progress on robustly extracting vascular networks from
50 imaging data and converting them into accurately segmented three-dimensional networks, see for
51 example Gould et al. (2017), acquiring large volumes of such data remains a time-consuming and
52 expensive task that can only be undertaken with considerable expertise. The strong dependence of
53 vessel resistance on vessel radius means that accurate values of the vessel diameter are critical if the
54 flow field is to be calculated accurately. The strong dependence of the chosen boundary conditions
55 on the flow simulations has also been noted by many authors, for example Lorthois et al. (2011).

56 These factors, together with the high vessel density that means that solving the flow field in volumes
57 of tissue that are of the length scale of a human imaging voxel (of order 1 mm) is highly
58 computationally challenging, has driven the development of homogenisation techniques based on
59 the creation of artificial networks that match experimentally measured properties, Su et al. (2012),
60 El-Bouri and Payne (2015) and El-Bouri and Payne (2016), and coupling these with models over
61 multiple length scales, El-Bouri and Payne (2018). These techniques enable a scaling up of networks
62 to a voxel scale and hence the flow fields can be related to imaging data, most easily through the use
63 of transit time distributions, see for example Park and Payne (2013). Other authors have developed
64 vascular networks through the use of bifurcating vessels, for example Boas et al. (2008) and Payne
65 and Lucas (2017), although in these models no spatial information is considered.

66 At a voxel level, the vasculature comprises vessels over a relatively wide range of length scales, with
67 diameters ranging from a few micrometres to hundreds of micrometres. Consideration does thus
68 need to be given to the assumptions and choice of equations that govern blood flow over these
69 length scales, in particular when attempting to bridge the 'imaging gap', when the assumptions valid
70 in the large vessels and those in the microvasculature may be significantly different. At the smallest
71 length scales, nearly all authors use the Poiseuille equation in some form, with viscosity either taken

72 to be constant, based on vessel diameter or based on vessel diameter and haematocrit, as shown in
 73 Table 1. In the latter two cases, empirical relationships are normally used, with a variety of different
 74 relationships having been applied. Once the resistance to flow is known, then the network reduces
 75 to a conductance matrix, which can be solved numerically, either by simple inversion for networks
 76 with constant haematocrit or by iteration for networks with non-constant haematocrit. It is usually
 77 assumed that at small length scales static pressure is conserved at nodes, as has been done in all the
 78 studies listed thus far.

79 Most of the models listed in Table 1 assume steady state flow conditions, with only a few
 80 considering the dynamic response, although this plays an important part in interpreting the
 81 response to changes in neural activity. Only the models by Boas et al. (2008), Reichold et al. (2009),
 82 Gagnon et al. (2015) and Payne and Lucas (2017) consider the dynamic response of the small vessels
 83 in the cerebral vasculature. These mostly assume a non-linear compliance of the vessels, enabling
 84 changes in flow to drive changes in volume. Such changes in blood volume are of particular
 85 importance in the context of imaging techniques such as the BOLD response, where short-term
 86 changes in blood volume can strongly influence the response.

Model	Static/dynamic	Flow model	Viscosity model
Fang et al. (2008)	Static	Poiseuille equation	Constant
Boas et al. (2008)	Dynamic	Poiseuille equation and non-linear compliance	Pries et al. (1992), with haematocrit as function of diameter
Reichold et al. (2009)	Dynamic	Poiseuille equation and non-linear compliance	Pries et al. (1992), with haematocrit as function of diameter
Guibert et al.	Static	Poiseuille equation	Kiani and Hudetz (1991) or Pries

(2010)			and Secomb (2005), with haematocrit model
Lorthois et al. (2011)	Static	Poiseuille equation	Pries et al. (1996), with haematocrit model
Safaeian et al. (2011)	Static	Poiseuille equation	Pries and Secomb (2005), with haematocrit model
Linninger et al. (2013)	Static	Poiseuille equation	Pries et al. (1996), with constant haematocrit
Gagnon et al. (2015)	Dynamic	Poiseuille equation and non-linear compliance	Pries et al. (1990), 'corrected for haematocrit'
Gould et al. (2017)	Static	Coupled model of flow and haematocrit, rigid vessels	Plasma skimming model
Schmid et al. (2017)	Static	Poiseuille equation	Pries et al. (1992), with tracking of red blood cells
Payne and Lucas (2017)	Dynamic	Poiseuille equation	Pries et al. (1992), with constant haematocrit
El-Bouri and Payne (2018)	Static	Poiseuille equation	Pries et al. (1992), with constant haematocrit

87 **Table 1** Summary of network models of cerebral blood flow and assumptions used

88 Other approaches have taken a more 'top-down' methodology, where lumped parameter models
89 (e.g. windkessel models) are used, with the lumped parameters aiming to capture the overall
90 behaviour of flow through large numbers of vessels in a very small number of parameters, see for
91 example those used by Ress et al. (2009), Kim et al. (2013) in the context of models of oxygen
92 delivery, and Buxton et al. (1998) and many subsequent studies (for example Aquino et al. (2014)) in
93 the context of models of the BOLD response. Such models have a valuable role to play in

94 understanding the behaviour at large scales, but are inevitably limited by both their simplicity and
95 the difficulties involved in linking the model parameters to the underlying network physiology.

96 The assumptions made are often very different in models of flow in the larger vessels, for example
97 when the dynamic behaviour of the flow field plays an important part in both flow and volume, and
98 when total pressure is often conserved at nodes, see for example Alastruey et al. (2007). In order to
99 link models across the ‘imaging gap’, care has to be taken and the limits of assumptions fully
100 understood. For a comprehensive review of models of cerebral blood flow, the reader is referred to
101 Payne (2017).

102 In this paper we thus consider the modelling of cerebral blood flow and volume in networks of blood
103 vessels in detail, justify suitable approximations that can be made, and propose a framework that
104 can be used that is mathematically rigorous and computationally simple. We will also consider the
105 limits of the approximations and hence illustrate how models can be developed that will cover
106 multiple scales. In order to do this, we consider the governing equations and use these to develop a
107 model relating blood flow and volume to pressure in a single vessel; finally we link vessels together
108 within a network and then show how the equations can be solved dynamically within a network. In
109 the last section we will consider each of these in turn before illustrating our proposed approach in
110 the context of the cerebral vasculature, comparing simulation results with those obtained using
111 previous approaches.

112 **2 Theory**

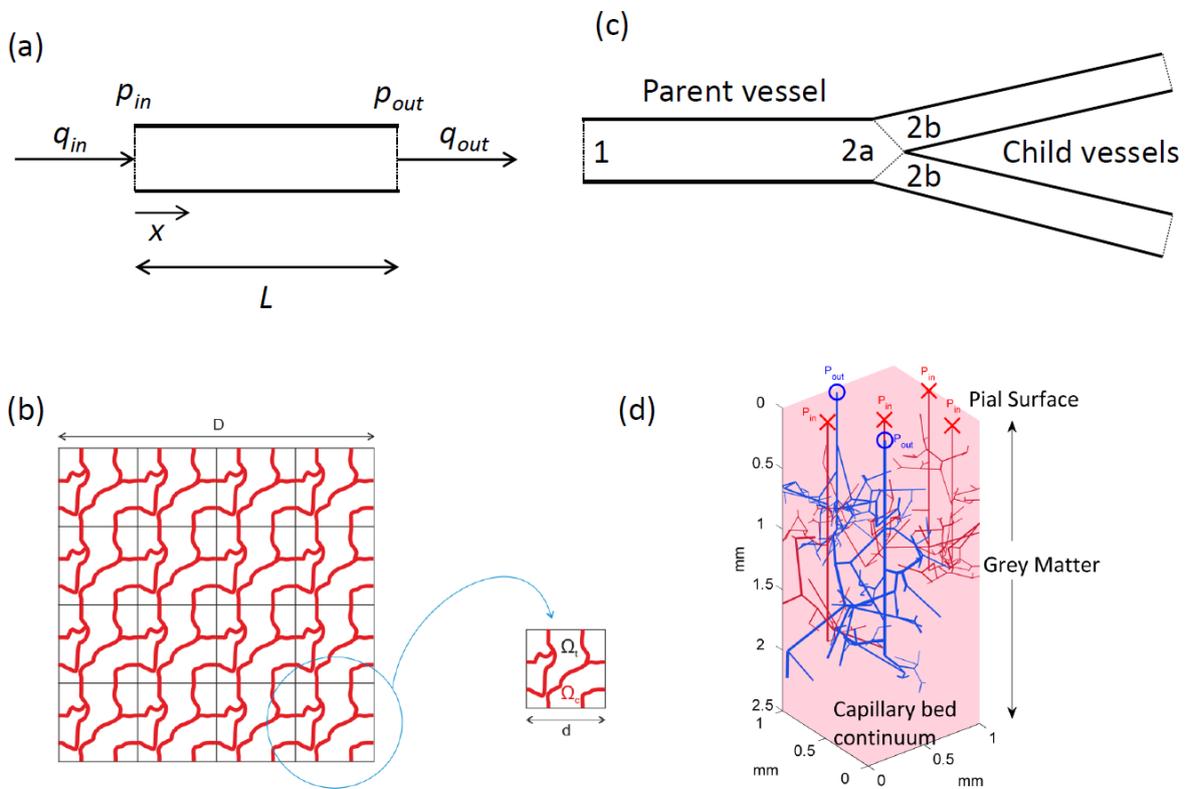
113 We assume blood to be a Newtonian fluid of viscosity μ and density ρ in a flow field that is governed
114 by the incompressible form of the Navier-Stokes equations. These fundamental fluid flow equations
115 are based on the concepts of conservation of mass and balance of forces; a full explanation and
116 derivation can be found in many sources, see for example Acheson (1990). Hence:

$$117 \quad \frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} = -\frac{1}{\rho} \nabla p + \frac{\mu}{\rho} \nabla^2 \mathbf{u} \quad (1)$$

118 with velocity field \mathbf{u} driven by a pressure field p . In an axisymmetric vessel this reduces to:

119
$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mu}{\rho} \nabla^2 u \quad (2)$$

120 where the flow velocity has only an axial component, u , which is a function of radius, r , axial position,
 121 x , and time, t . In this latter case, the pressure gradient can be shown to be only a function of axial
 122 position and time, i.e. the pressure is uniform over the cross-sectional area, based on order of
 123 magnitude arguments, Canic and Kim (2003). A similar order of magnitude argument can be used to
 124 neglect the radial component of the velocity field when the variations in the vessel cross-section are
 125 not too fast, Canic and Kim (2003). We note that the assumption of a Newtonian fluid is a limitation
 126 to this analysis, but one that we will consider more fully in the Discussion. For ease of reference,
 127 schematics of the different components of the model are shown in Figure 1, to which we refer
 128 throughout.



129

130 **Figure 1** Schematic of components of model: (a) single vessel model; (b) continuum model; (c) node
 131 model; (d) coupled penetrating vessel and capillary bed continuum model. Figures (b) and (d)
 132 reproduced from El-Bouri (2017)

133 **2.1 Result 1: The advection term can be neglected when $\frac{E}{\rho U^2} \frac{h}{R} \gg \frac{3}{2}$ (E is Young's modulus, ρ is fluid
 134 density, U is flow velocity, h is wall thickness and R is vessel inner radius)**

135 The first result that we show is that the advection term can be neglected in models of cerebral blood
 136 flow when the vessel wall stiffness scaled by wall thickness to radius ratio is greater than a multiple
 137 of the dynamic head. This result is required first to enable us to write down the governing equations
 138 in a simplified form so that we can derive a model for the inlet and outlet flows in the next section.

139 We will demonstrate this in two parts. We first consider the flow in individual vessels, Figure 1a,
 140 since a simple result can be obtained, before considering the flow field across multiple scales, Figure
 141 1b. This latter approach allows us to consider the flow field as a whole; this is valuable since it links
 142 to previous work that has shown how the flow field in the capillary vessels can be modelled using
 143 homogenisation, El-Bouri and Payne (2015). For simplicity we only consider the steady state solution,
 144 but this does not affect the result.

145 **Single vessels**

146 We firstly reduce the steady state form of Equation 2 to non-dimensional form, where we reference
 147 velocity and pressure to characteristic values, U and P respectively:

$$148 \quad u^* \frac{\partial u^*}{\partial x^*} = - \left(\frac{P}{\rho U^2} \right) \frac{\partial p^*}{\partial x^*} + \frac{1}{Re_L} \nabla^2 u^* \quad (3)$$

149 where the star is used here to denote a value as a fraction of its characteristic value, i.e. $u^* = u/U$,
 150 $p^* = p/P$ and $x^* = x/L$, and noting that we do not assume any relationship between characteristic
 151 pressure and characteristic velocity, retaining generality at this stage. The co-ordinate x is

152 referenced to vessel length, L (and hence the ∇^2 operator is also made non-dimensional with respect
153 to L). Note that Reynolds number in Equation 3 is based on vessel length:

$$154 \quad Re_L = \frac{\rho UL}{\mu} \quad (4)$$

155 We use a subscript for Reynolds number throughout to make it clear what length scale is being used.
156 The aim is then to consider the relative magnitudes of the advection and pressure gradient terms,
157 since these are the two terms with first order axial derivative terms and thus terms that can be
158 compared directly through order of magnitude arguments.

159 Conservation of mass, averaged over the cross-sectional area, gives:

$$160 \quad \frac{\partial A}{\partial t} + \frac{\partial q}{\partial x} = 0 \quad (5)$$

161 where the flow rate, q , is the integral of the axial velocity over the cross-sectional area: see Canic
162 and Kim (2003) for a formal derivation of this result. In the steady state this reduces to a flow rate
163 that is invariant over axial length, as expected. Hence:

$$164 \quad A = \frac{q}{\bar{U}} \quad (6)$$

165 where the area-averaged velocity is given by \bar{U} (which can vary along the vessel). We next assume
166 that a relationship can be formulated between steady state pressure and cross-sectional area
167 (without at this stage specifying its form), i.e. $p = p(A)$. We neglect any viscous component of the
168 wall response here as we are only considering the steady state behaviour: note, however, that we
169 retain the viscous behaviour of the fluid, which means that the pressure will drop in the direction of
170 flow and hence the cross-sectional area of the vessel will also change in order to maintain flow rate.
171 We also neglect any axial stiffness, only considering the radial stiffness, as is commonly done, for
172 simplicity.

173 Using this assumption, Equations 3 and 6 yields:

174
$$u^* \frac{\partial u^*}{\partial x^*} = \left[A \frac{dp}{dA} \left(\frac{1}{\rho U^2} \right) \frac{U}{\bar{U}} \right] \frac{\partial \bar{U}^*}{\partial x^*} + \frac{1}{Re_R(R/L)} \nabla^2 u^* \quad (7)$$

175 where Reynolds number in Equation 7 is now based on vessel radius and this is scaled by the ratio of
 176 vessel radius to length (R/L). The key parameter is then the square bracket, since if this is much
 177 larger than 1, the advection term can be neglected in comparison with the pressure gradient term
 178 (note that although the derivatives are of different velocity terms, one being velocity as a function of
 179 radius and one the area-averaged velocity, they are of the same order of magnitude).

180 We therefore need to consider the pressure-area relationship more closely. Many different forms
 181 have been proposed for this, for example those by Langewouters et al. (1984), Stergiopoulos et al.
 182 (1992) and Formaggia et al. (1999). For simplicity we use the relationship that results from assuming
 183 static radial equilibrium of an isotropic elastic material with Young's modulus E , Poisson ratio
 184 ν , reference wall thickness h_{ref} and radius R_{ref} , as quoted by Formaggia et al. (1999) and widely
 185 used elsewhere:

186
$$p - p_{ref} = \frac{E h_{ref}}{R_{ref} (1 - \nu^2)} \left(\sqrt{\frac{A}{A_{ref}}} - 1 \right) \quad (8)$$

187 where the wall stiffness relates changes in pressure relative to a reference value, p_{ref} , to changes in
 188 cross-sectional area relative to a reference value, $A_{ref} = \pi R_{ref}^2$. Note that this model assumes that
 189 there is no axial stiffness: the wall thus responds at each axial location to the pressure at that
 190 location without reference to the remainder of the pressure field. More sophisticated models have
 191 been used, see for example Pedrizzetti and Perktold (2003), but this assumption is very commonly
 192 made in models of blood flow and is sufficient for the order of magnitude argument being made
 193 here.

194 This then gives:

195
$$\left[A \frac{dp}{dA} \left(\frac{1}{\rho U^2} \right) \bar{U} \right] = \frac{1}{2} \frac{E}{\rho U^2} \frac{h_{ref}}{R_{ref} (1 - \nu^2)} \sqrt{\frac{A}{A_{ref}}} \frac{U}{\bar{U}} \quad (9)$$

196 Since we can select the characteristic velocity to be close to the area-averaged value and assuming
 197 that all values are close to their reference value, this simplifies to give:

198
$$\left[A \frac{dp}{dA} \left(\frac{1}{\rho U^2} \right) \bar{U} \right] \approx \frac{2}{3} \frac{E}{\rho U^2} \frac{h}{R} \quad (10)$$

199 where we also assume a value of Poisson ratio of 0.5, denoting an incompressible material, as is
 200 commonly done. For advection to be neglected, this term must be significantly greater than 1, hence

201 $\frac{E}{\rho U^2} \frac{h}{R} \gg \frac{3}{2}$. We will examine this result again in the context of the cerebral vasculature later.

202 Note that although we have only considered the steady state response here, the result is also valid
 203 for dynamic flow fields, since we have compared the two terms with first order axial derivatives and
 204 thus including dynamic terms in the equations will not affect the validity of this particular result. It
 205 would be worth considering in future the relative magnitudes of the acceleration term and the
 206 viscous wall behaviour (the two terms with first order time derivatives). It should be noted, however,
 207 that the available data for visco-elastic models of the vessel wall in the cerebral vasculature are very
 208 sparse.

209 **Continuous flow field**

210 Having considered the flow in individual vessels above, we next show how the advection term can be
 211 neglected when considering the flow field as a continuous one. This approach is based on the
 212 method set out by Shipley and Chapman (2010) and previously adapted for the cerebral
 213 microcirculation by El-Bouri and Payne (2015). We include this analysis since we have previously
 214 shown how the flow field within volumes of brain tissue can be modelled using a coupled approach
 215 that incorporates both the flow in individual non-capillary vessels and a Darcy flow for the capillary

216 vessels, El-Bouri and Payne (2018), and thus wish to show that the advection term can be neglected
217 when considering the flow field as a continuum.

218 As before, we consider the solution in the steady state but start from the Navier-Stokes equations
219 for incompressible flow:

$$220 \quad (\mathbf{u}_c \cdot \nabla) \mathbf{u}_c = -\frac{1}{\rho} \nabla p_c + \frac{\mu}{\rho} \nabla^2 \mathbf{u}_c \text{ in } \Omega_c \quad (11)$$

221 where the velocity field in the capillary domain, Ω_c , is given by \mathbf{u}_c . The boundary conditions are as
222 given in El-Bouri and Payne (2015): however, since we are not attempting to solve the equations
223 here, we will not consider the boundary conditions further as they are not directly relevant to the
224 derivation below. We define a small parameter $\varepsilon = d/D$ that relates the micro length scale, d , to
225 the macro length scale, D , as shown in Figure 1b (note that this definition of ε is only used in this
226 section).

227 We reduce the equations to non-dimensional form using the following scaling:

$$228 \quad \mathbf{u}_c = U \mathbf{u}_c^* \quad (12)$$

$$229 \quad p = \frac{\mu D U}{d^2} p^* + p_0 \quad (13)$$

$$230 \quad \mathbf{X} = d \mathbf{X}^* \quad (14)$$

231 based on a characteristic velocity U , capillary length scale d , voxel length scale D , and a characteristic
232 pressure that is based on viscous forces with an arbitrary offset. This scaling of pressure is based on
233 the fact that viscous forces dominate at the local scale and thus to bring the characteristic value of
234 pressure to the macro scale it is rescaled by ε^{-2} : this is due to the fact that the inter-capillary
235 spacing is of order ε and so there are of order ε^2 capillaries per unit area, meaning that pressure
236 scales with ε^{-2} . These characteristic values reduce Equation 11 to the following (where we drop the
237 star notation straight away for ease of notation):

238
$$\varepsilon Re_d (\mathbf{u}_c \cdot \nabla) \mathbf{u}_c = -\nabla p_c + \varepsilon \mu \nabla^2 \mathbf{u}_c \quad (15)$$

239 where Reynolds number on the micro scale is defined as:

240
$$Re_d = \frac{\rho U d}{\mu} \quad (16)$$

241 and the Reynolds number on the macro scale is therefore equal to $Re_D = Re_d / \varepsilon$. Since the problem
242 is more commonly formulated in terms of this parameter, Equation 15 thus becomes:

243
$$\varepsilon^2 Re_D (\mathbf{u}_c \cdot \nabla) \mathbf{u}_c = -\nabla p_c + \varepsilon \mu \nabla^2 \mathbf{u}_c \quad (17)$$

244 Since we consider the capillary bed relative to the larger vessels here, this gives micro and macro
245 length scales of approximately 100 μm and 1 cm respectively (noting that this analysis can be applied
246 to any separation of scales where the parameter ε is small). In this case, this parameter is equal to
247 approximately 0.01. For typical values of blood viscosity and density (3 mPa.s and 1040 kg/m³
248 respectively), the macro Reynolds number is of order 1, where we assume a capillary velocity of
249 order 1 mm/s, see for example Unekawa et al. (2010). There is thus no need to re-scale Equation 17.
250 We now use a classical separation of scales approach. Since $\varepsilon \ll 1$, the local and macro length scales
251 are well separated and can be defined as \mathbf{X} and $\mathbf{x} = \varepsilon \mathbf{X}$. Hence, using the standard approach, see for
252 example Holmes (2013), for separation of scales:

253
$$\nabla = \nabla_X + \varepsilon \nabla_x \quad (18)$$

254
$$\nabla^2 = \nabla_X^2 + 2\varepsilon \nabla_x \cdot \nabla_X + \varepsilon^2 \nabla_x^2 \quad (19)$$

255 and a multiple scales expansion:

256
$$\mathbf{u}_c = \mathbf{u}_c^0(\mathbf{x}, \mathbf{X}) + \varepsilon \mathbf{u}_c^1(\mathbf{x}, \mathbf{X}) + \varepsilon^2 \mathbf{u}_c^2(\mathbf{x}, \mathbf{X}) + \dots \quad (20)$$

257
$$p = p^0(\mathbf{x}, \mathbf{X}) + \varepsilon p^1(\mathbf{x}, \mathbf{X}) + \varepsilon^2 p^2(\mathbf{x}, \mathbf{X}) + \dots \quad (21)$$

258 Substituting Equations 18-21 into the governing equation (Equation 17) orders of ε can now be
259 compared.

260 First in ε^0 :

$$261 \quad \nabla_x p^0 = 0 \quad (22)$$

262 and then in ε^1 :

$$263 \quad \nabla_x p^1 + \nabla_x p^0 = \nabla_x^2 \mathbf{u}_c^0 \quad (23)$$

264 Equations 22 and 23 can be solved along the lines proposed by Shipley and Chapman (2012) and as
265 performed in the cerebral microvasculature by El-Bouri and Payne (2015): these two equations are
266 sufficient to solve to leading order. The full derivation is given in Appendix A, with the end result
267 being a volume-averaged Darcy equation:

$$268 \quad \langle \mathbf{u}_c^{(0)} \rangle_{\Omega_c} = -\mathbf{K} \nabla_x p_c^{(0)} \quad (24)$$

269 where the permeability tensor, \mathbf{K} , is given in full in Appendix A. The advection term thus plays no
270 role in this context at leading order and can be considered only as a small correction term.

271 These two results thus combine to show that the advection term can be neglected in both individual
272 vessels (under the condition given above) and in the microvasculature when treated as a continuum.
273 This is a very important result, as it removes the only non-linear term in the Navier-Stokes equations.
274 Based on this result, we can utilise a wide range of results based on linear theory. It is worth noting
275 in passing that a number of authors have neglected the advection term by linearizing the governing
276 equations about a zero mean velocity, see for example Flores et al. (2016). Although the final result
277 obtained is the same, this linearization is, strictly speaking, unnecessary and can appear to limit the
278 validity of the solution. The results above offer a more rigorous and general proof that has a simple
279 condition: one that we will examine in more detail in the context of the cerebral circulation later.

280 **2.2 Result 2: A first order differential model relating inlet and outlet flows to inlet and outlet**
 281 **pressures in a vessel can be used when $\alpha < 1$ (α is Womersley number)**

282 Having considered the flow as continuous in the second half of the result above, we now return to
 283 consideration of a single vessel, as shown in Figure 1a. The aim here is to solve for the flow field such
 284 that a relationship can be derived between the inlet and outlet flows and the inlet and outlet
 285 pressures. In this way a simple relationship can be used for the flow in and out of each vessel in a
 286 network such that a network of vessels can be connected together, using the results presented later.
 287 In Result 1, we showed that the advection term can be neglected. As a result the governing
 288 equations for flow in a single compliant vessel (the area-averaged Navier-Stokes equations coupled
 289 with an elastic wall model) reduce to a linear form, enabling them to be transformed into the
 290 frequency domain and written in the following form:

291
$$\hat{p}'' = \left(\frac{i\omega ZC}{L^2} \right) \hat{p} \quad (25)$$

292 where:

293
$$Z = \mathcal{R} \frac{i\alpha^2}{8} \left[1 - \frac{2 J_1(\alpha i^{3/2})}{\alpha i^{3/2} J_0(\alpha i^{3/2})} \right]^{-1} \quad (26)$$

294 and impedance, Z , resistance, \mathcal{R} , and compliance, C , are defined here for the whole vessel, of length
 295 L . J_0 and J_1 denote Bessel functions of the first kind. We omit the dependence on frequency for
 296 clarity, since the overhat denotes that the variable has been transformed into the frequency domain.
 297 Womersley number is denoted by $\alpha = R\sqrt{\omega/\nu}$ and can be considered to be the ratio of oscillatory
 298 inertial forces to shear forces. The derivation for these equations is based on the results of
 299 Womersley (1955) and can be found in full in Flores et al. (2016). A schematic of the single vessel
 300 model is shown in Figure 1a: we now consider this single vessel in this section without further
 301 reference to the continuum model.

302 We can then use a perturbation series for pressure:

$$303 \quad \hat{p} = \hat{p}_0 + \varepsilon \hat{p}_1 + \varepsilon^2 \hat{p}_2 \dots (27)$$

304 in the small parameter, ε , defined in this section as:

$$305 \quad \varepsilon = \alpha i^{3/2} (28)$$

306 We will examine the magnitude of this parameter later, but note that for the moment we are simply
307 assuming that it has magnitude less than one. Note that this is a different definition for ε from that
308 used in Section 2.1: we use this definition here as it is the standard notation for perturbation
309 methods and thus enables results obtained here to be easily compared with equivalent results
310 elsewhere.

311 Substituting Equation 28 into Equation 26 and Equations 26 and 27 into Equation 25 then yields:

$$312 \quad [\varepsilon J_0(\varepsilon) - 2J_1(\varepsilon)](\hat{p}_0'' + \varepsilon \hat{p}_1'' + \varepsilon^2 \hat{p}_2'' \dots) = \varepsilon^5 \left(\frac{\nu \mathcal{R} C}{8L^2 R^2} \right) J_0(\varepsilon) (\hat{p}_0 + \varepsilon \hat{p}_1 + \varepsilon^2 \hat{p}_2 \dots) (29)$$

313 We next convert the variables to non-dimensional form, such that pressure is computed relative to a
314 reference value (the value of this is irrelevant, since both sides of Equation 29 are linearly
315 proportional to pressure) and length relative to the length of the vessel, L . The prime thus becomes
316 relative to fractional length along the vessel. The problem is then defined in just two parameters, ε ,
317 and:

$$318 \quad \beta = \frac{\nu \mathcal{R} C}{8R^2} (30)$$

319 where resistance and compliance are equal to:

$$320 \quad \mathcal{R} = \frac{8\mu L}{\pi R^4} (31)$$

$$321 \quad C = L \frac{dA}{dp} (32)$$

322 The non-dimensional parameter β is of similar form to the (inverse square of) Womersley number,
 323 but based on the time constant of the vessel (where $T = \mathcal{RC}$, as defined later) rather than the
 324 oscillation frequency. The behaviour of each vessel is thus governed by the relative magnitudes of
 325 these two non-dimensional groups.

326 To calculate the pressure series, we next use the series expansion of the Bessel functions,
 327 Abramowitz and Stegun (1964):

$$328 \quad J_0(x) = \sum_{i=0}^{\infty} \frac{(-1)^k}{2^{2k}(k!)^2} x^{2k} = 1 - \frac{x^2}{4} + \frac{x^4}{64} - \frac{x^6}{2304} + \dots \quad (33)$$

$$329 \quad J_1(x) = \sum_{i=0}^{\infty} \frac{(-1)^k}{2^{2k+1}k!(k+1)!} x^{2k+1} = \frac{x}{2} - \frac{x^3}{16} + \frac{x^5}{384} - \frac{x^7}{18432} + \dots \quad (34)$$

330 Balancing terms in ascending powers of ε gives:

$$331 \quad \hat{p}_0'' = 0 \quad (35)$$

332 which means that the pressure field to zeroth order is linear, set by the inlet and outlet boundary
 333 conditions, as would be expected;

$$334 \quad \hat{p}_1'' = 0 \quad (36)$$

335 which means that the first order pressure field is zero everywhere, since the inlet and outlet
 336 boundary conditions at first and higher orders are zero;

$$337 \quad \hat{p}_2'' = -8\beta\hat{p}_0 \quad (37)$$

338 which can be solved as described below;

$$339 \quad \hat{p}_3'' = 0 \quad (38)$$

340 which means that the third order pressure field is also zero everywhere; and

341
$$\hat{p}_4'' = -8\beta \left[\hat{p}_2 - \frac{1}{6}\hat{p}_0 \right] \quad (39)$$

342 We can now proceed to solve for the pressure field in the vessel up to this order. Equation 35 can be
 343 solved using the inlet and outlet boundary conditions, defined here to be:

344
$$\hat{p}_0(x = 0) = \hat{p}_{in} \quad (40)$$

345
$$\hat{p}_0(x = 1) = \hat{p}_{out} \quad (41)$$

346 noting that these boundary conditions can of course be dynamically varying, since this is the solution
 347 in the frequency domain, which can easily be inverted into the time domain. The zeroth order
 348 pressure field is:

349
$$\hat{p}_0 = \hat{p}_{in}(1 - x) + \hat{p}_{out}x \quad (42)$$

350 The resulting second order expression is calculated by substitution of Equation 42 into Equation 37
 351 and solving given zero boundary conditions:

352
$$\hat{p}_2 = \hat{p}_{in} \frac{4\beta}{3} x(1 - x)(2 - x) + \hat{p}_{out} \frac{4\beta}{3} x(1 - x^2) \quad (43)$$

353 and the fourth order expression similarly using Equations 42, 43 and 39:

354
$$\hat{p}_4 = -8\beta \left[\hat{p}_{in}x(1 - x) \left\{ -\frac{\beta}{45}(3x^3 - 12x^2 + 8x - 8) + \frac{1}{36}(2 - x) \right\} \right.$$

 355
$$\left. + \hat{p}_{out}x(1 - x) \left\{ \frac{\beta}{45}(3x^3 + 3x^2 - 7x - 7) + \frac{1}{36}(1 + x) \right\} \right] \quad (44)$$

356 The full solution is then:

357
$$\hat{p} = \hat{p}_0 + \varepsilon^2 \hat{p}_2 + \varepsilon^4 \hat{p}_4 \dots \quad (45)$$

358 It should be noted that the expansion has been performed in terms of ε , but gives an expansion in
 359 terms of even powers of ε , where ε is proportional to the square root of frequency: hence the
 360 expansion is in integer powers of frequency.

361 Given the solution for the pressure field in the vessel, the flow field in the vessel can be calculated.

362 This is most easily done using a second perturbation series for flow of the form:

$$363 \quad \hat{q} = \hat{q}_0 + \varepsilon \hat{q}_1 + \varepsilon^2 \hat{q}_2 \dots (46)$$

364 where we substitute this into the expression for impedance:

$$365 \quad \hat{q} = -\frac{1}{Z} \hat{p}' (47)$$

366 where the impedance is given by Equation 26 and the pressure by Equation 45, to obtain an

367 expression along the lines of Equation 29. We then calculate the flow field by balancing terms in

368 powers of ε , as done for the pressure field earlier, to give:

$$369 \quad \hat{q}_0 = -\frac{1}{\mathcal{R}} \hat{p}'_0 (48)$$

$$370 \quad \hat{q}_2 = -\frac{1}{\mathcal{R}} \left[\hat{p}'_2 + \frac{1}{6} \hat{p}'_0 \right] (49)$$

$$371 \quad \hat{q}_4 = -\frac{1}{\mathcal{R}} \left[\hat{p}'_4 + \frac{1}{6} \hat{p}'_2 + \frac{11}{384} \hat{p}'_0 \right] (50)$$

372 where the differentials are again relative to non-dimensional length. Equations 42-44 can then be

373 substituted into these equations to derive an expression for the whole flow field. Most usefully,

374 however, the inlet and outlet flows can be calculated in terms of the inlet and outlet pressures. Since

375 these are linear, they are most easily written in matrix form:

$$376 \quad \begin{pmatrix} \hat{q}_{in} \\ \hat{q}_{out} \end{pmatrix} = \alpha_0 \begin{pmatrix} \hat{p}_{in} \\ \hat{p}_{out} \end{pmatrix} + \alpha_2 \varepsilon^2 \begin{pmatrix} \hat{p}_{in} \\ \hat{p}_{out} \end{pmatrix} + \alpha_4 \varepsilon^4 \begin{pmatrix} \hat{p}_{in} \\ \hat{p}_{out} \end{pmatrix} + \dots (51)$$

377 where:

$$378 \quad \alpha_0 = \frac{1}{\mathcal{R}} \begin{pmatrix} 1 & -1 \\ 1 & -1 \end{pmatrix} (52)$$

$$379 \quad \alpha_2 = \frac{1}{6\mathcal{R}} \begin{pmatrix} 1 & -1 \\ 1 & -1 \end{pmatrix} + \frac{4\beta}{3\mathcal{R}} \begin{pmatrix} -2 & -1 \\ 1 & 2 \end{pmatrix} (53)$$

380
$$\alpha_4 = \frac{11}{384} \frac{1}{\mathcal{R}} \begin{pmatrix} 1 & -1 \\ 1 & -1 \end{pmatrix} + \frac{4\beta}{9\mathcal{R}} \begin{pmatrix} 2 & 1 \\ -1 & -2 \end{pmatrix} + \frac{8\beta^2}{45\mathcal{R}} \begin{pmatrix} -8 & -7 \\ 7 & 8 \end{pmatrix} \quad (54)$$

381 At zeroth order, i.e. steady state, the solution is exactly matched with the Poiseuille flow solution, i.e.
 382 the inlet and outlet flows are equal to the driving pressure divided by the vessel resistance. The
 383 Poiseuille solution is thus the leading order term in the dynamic solution. The second order
 384 component of the solution (linearly proportional to frequency) then provides a dynamic ‘correction’
 385 that is dependent upon the non-dimensional group defined by Equation 30. This term is in turn
 386 dependent upon both the vessel resistance and the compliance and hence dependent on both the
 387 fluid and vessel properties. Note that the inlet and outlet can be swapped round and the formulation
 388 will remain the same, as would be expected given the original equations. The fourth order
 389 component is proportional to the square of frequency and can be neglected to a high degree of
 390 accuracy (it is included here primarily for use in the following section).

391 As well as the frequency domain representation, it is useful to consider the results back in the time
 392 domain. Considering Equation 51 and truncating the solution after terms up to ε^2 gives:

393
$$\begin{pmatrix} q_{in} \\ q_{out} \end{pmatrix} = \alpha_0 \begin{pmatrix} p_{in} \\ p_{out} \end{pmatrix} - \frac{R^2}{v} \alpha_2 \frac{d}{dt} \begin{pmatrix} p_{in} \\ p_{out} \end{pmatrix} \quad (55)$$

394 These (first-order differential) equations can then be used to relate the flows and pressures in each
 395 vessel in a network, based on the two parameters β and \mathcal{R} , calculated for each vessel, by
 396 substituting in the expressions for α_0 and α_2 given in Equations 52 and 53 respectively. For example,
 397 in a single vessel, the inlet and outlet flows can be calculated directly from the inlet and outlet
 398 pressures using Equation 55 and specific values of the two parameters. For a single vessel, the model
 399 can be represented using two 2x2 matrices, relating the flows to the pressures; with the addition of
 400 each vessel to a network, an additional unknown variable will be added, increasing the size of the
 401 matrices by 1 in each dimension. This can then be done up to a network of arbitrary size, although it
 402 is likely that alternative mathematical formulations would be used in very large networks due to the
 403 computational cost.

404 For most networks this will be a sufficient representation, without the need for further terms: the
 405 first term on the left hand side of Equation 55 is the ‘traditional’ term that relates steady flow to a
 406 steady pressure difference along the vessel, with the second term adding in the dynamic effects that
 407 occur due to the oscillation of the fluid and the interaction between the unsteady fluid motion and
 408 an elastic wall. Note that the dynamic term thus exists even in a rigid vessel. We will consider in
 409 more detail how these equations can be linked together later, once we have considered the
 410 equations for volume and for connecting vessels in the next two sections, and then give an example
 411 of the solution obtained using this approach.

412 **2.3 Result 3: Blood volume can be modelled as quasi-steady-state when $\omega T \ll 180$ (ω is driving**
 413 **frequency, T is vessel time constant)**

414 In the previous result, we derived a relationship between the inlet and outlet flows and the driving
 415 pressures in a single vessel, Figure 1a. This enables us directly to consider changes in the volume of
 416 the vessel, V , through the difference between inlet and outlet flows:

417
$$\frac{dV}{dt} = q_{in} - q_{out} \quad (56)$$

418 In the frequency domain, using Equation 51 and Equation 56 gives:

419
$$i\omega\hat{V} = -4\frac{\beta}{\mathcal{R}}\varepsilon^2(1-1)\left(\hat{p}_{in}\right) + \varepsilon^4\frac{4\beta}{9\mathcal{R}}\left(1-\frac{2}{5}\beta\right)(1-1)\left(\hat{p}_{in}\right) + \dots \quad (57)$$

420 Substituting in Equation 28 and dividing by $i\omega$ (i.e. integrating) then gives:

421
$$\hat{V} = \frac{C}{2}(\hat{p}_{in} + \hat{p}_{out}) + i\omega\frac{R^2}{18\nu}\left(1-\frac{2}{5}\beta\right)C(\hat{p}_{in} - \hat{p}_{out}) + \dots \quad (58)$$

422 Hence to first order, the volume is equal to the product of compliance with average pressure, as
 423 expected. The second term in Equation 58 is the dynamic component of volume changes: this is
 424 particularly important in the context of localised changes in flow in response to activation. This

425 second term can be considered to be a ‘dynamic’ compliance term. If we assume that β is large
 426 (strictly much larger than 5/2), then Equation 58 approximates to:

$$427 \quad \hat{V} = \frac{C}{2}(\hat{p}_{in} + \hat{p}_{out}) - i\omega \frac{\beta R^2}{45\nu} C(\hat{p}_{in} - \hat{p}_{out}) + \dots \quad (59)$$

428 We then formally define the product of resistance and compliance to be the time constant of the
 429 vessel:

$$430 \quad T = \mathcal{R}C \quad (60)$$

431 and hence Equation 59 simplifies to (eliminating β using Equation 30):

$$432 \quad \hat{V} = \frac{C}{2} \left[(\hat{p}_{in} + \hat{p}_{out}) - \frac{i\omega T}{180} (\hat{p}_{in} - \hat{p}_{out}) + \dots \right] \quad (61)$$

433 Hence, the dynamic component can be neglected when $\omega T \ll 180$. Note that in the case where β is
 434 not much larger than 5/2, then the dynamic component in Equation 58 will depend primarily on the
 435 square of Womersley number, which then should be much less than 18 for the dynamic component
 436 to be negligible: since we have already discussed this in Section 2.3, we will not consider this case
 437 further. For completeness, as in the previous section, we convert Equation 61 back to the time
 438 domain:

$$439 \quad V = \frac{C}{2} \left[(p_{in} + p_{out}) - \frac{T}{180} \frac{d}{dt} (p_{in} - p_{out}) + \dots \right] \quad (62)$$

440 However, under the condition above ($\omega T \ll 180$), the volume then essentially follows a quasi-
 441 steady state dependence on the average pressure in the vessel as follows:

$$442 \quad V = \frac{C}{2} (p_{in} + p_{out}) \quad (63)$$

443 Note of course that we have not considered the viscoelastic nature of the vessel wall, which would
 444 of course influence the result; however, the oscillation of the fluid makes only a negligible
 445 contribution to the effective compliance of the vessel under this condition.

446 **2.4 Result 4: Matching of static pressure at nodes can be used when $\varepsilon Re_D \ll 100$ (ε is ratio of**
447 **vessel radius to length, Re_D is Reynolds number based on vessel diameter)**

448 In the previous two sections we have derived relationships for inlet and outlet flows and volume in a
449 single vessel as a function of the inlet and outlet pressures. The final stage in modelling the cerebral
450 vasculature is to connect the vessels together. The main consideration here is the choice of
451 boundary conditions relating flows and pressures at the nodes that connect individual vessels. Once
452 these have been determined, all of the flows and volumes can be determined.

453 The first boundary condition that is universally applied is conservation of flow at nodes, i.e. the flow
454 entering a node and the flow exiting a node must balance at all times. However, there is less
455 agreement over the second boundary condition, related to pressure; two approaches have been
456 used, essentially assuming that either static pressure remains the same as flow passes from one
457 vessel into the next (as the flow velocity changes, this means that energy is not conserved), or that
458 total pressure (and hence energy) is conserved, as discussed in the Introduction. The former
459 approach however has the advantage that it is a linear condition and thus results in less
460 computationally expensive numerical solutions. We thus examine in this section whether or not
461 there is a significant difference between the two approaches.

462 We consider a bifurcating node, as shown in Figure 1c, where a parent vessel supplies two child
463 vessels, where the inlet and outlet to the parent vessel are termed nodes 1 and 2a respectively, and
464 the inlet to both child vessels is termed node 2b, i.e. points 2a and 2b are taken to be immediately
465 before and after the node. If we assume identical conditions in both child vessels, the velocities are
466 in the ratio:

467
$$\frac{u_C}{u_P} = \frac{1}{2} \left(\frac{R_P}{R_C} \right)^2 \quad (64)$$

468 relative to that in the parent vessel, from conservation of flow, where the subscripts P and C refer to
 469 conditions in the parent and child vessels respectively. If we next assume Murray's law, Murray
 470 (1926), with exponent n , we can also calculate the ratio of the vessel radii:

$$471 \quad (R_p)^n = (R_c)^n + (R_c)^n = 2(R_c)^n \quad (65)$$

472 since we are assuming identical child vessels. Hence:

$$473 \quad \frac{u_c}{u_p} = \frac{1}{2} (2^{1/n})^2 = 2^{(-1+\frac{2}{n})} \quad (66)$$

474 Matching total pressure at the node gives:

$$475 \quad p_{2a} + \frac{1}{2} \rho u_p^2 = p_{2b} + \frac{1}{2} \rho u_c^2 \quad (67)$$

476 We can thus calculate the change in pressure across the node, i.e. from the outlet of the parent
 477 vessel to the inlet of the child vessel, as a fraction of the inlet velocity head:

$$478 \quad C_p = \frac{p_{2b} - p_{2a}}{\frac{1}{2} \rho u_p^2} = 1 - 2^{\frac{2(2-n)}{n}} \quad (68)$$

479 This is equal to 0 for $n = 2$, 0.18 for $n = 7/3$ and 0.37 for $n = 3$: these values being selected based on a
 480 number of studies that have examined the value of this exponent in a number of scenarios, see for
 481 example Mut et al. (2014). The largest value of this pressure coefficient is thus 0.37, which will tend
 482 to occur at the smallest length scales as this is where n is closest to 3. Note that it is of course also
 483 equal to 0 for the case of conservation of total pressure (the case where $n = 2$ is thus the only one
 484 where both are matched). Now compare this to the pressure loss due to friction in the parent vessel:

$$485 \quad C_p = \frac{p_1 - p_{2a}}{\frac{1}{2} \rho u_p^2} = \frac{32}{\varepsilon Re_D} \quad (69)$$

486 where Reynolds number is here based on the parent vessel diameter, similar to Equation 4, and:

487

$$\varepsilon = \frac{R_p}{L_p} \quad (70)$$

488

is the radius to length ratio of the parent vessel (note that we again use ε in this section with a

489

different definition from earlier). This calculation for head loss is based on the assumption of laminar

490

flow (a reasonable approximation in this context since Reynolds number is low), as outlined in

491

standard fluid mechanics texts, see for example Caro et al. (2012).

492

Since the largest head loss coefficient at a node (Equation 68) is equal to 0.37, as shown above, this

493

is only comparable in magnitude to the head loss coefficient for an individual vessel (Equation 69)

494

when the product εRe_D is approximately 100. Hence, if this product is less than 100, the difference

495

between assuming matched static pressure and matched total pressure is small, since the head loss

496

across the node is small in comparison with the head loss along the upstream vessel. Since the

497

matching of static pressure results in linear equations, this can be used under this condition to

498

simplify the solution procedure without significant loss of accuracy. The question of whether static

499

or total pressure should be matched in the vessels where this condition does not hold is a difficult

500

one and one that needs further investigation but which is outside the scope of this paper.

501

2.5 Result 5: Flow in a network can be solved using a series of matrices

502

Based on Result 4, we can assume matched static pressure at nodes without any significant loss of

503

accuracy if $\varepsilon Re_D < 100$. The resulting equations for a network, for example that shown in Figure 1d,

504

can then be expressed in matrix form:

505

$$\alpha_{int} \mathbf{p}_{int} = \alpha_{ext} \mathbf{p}_{ext} \quad (71)$$

506

in terms of the (unknown) pressures at the internal nodes and the (known) pressures at the external

507

nodes. Equation 71 holds separately for each order of the solution. Once the matrices have been

508

formulated, Equation 71 can be solved for the unknown internal node pressures separately for each

509

order and the flows calculated through each vessel using the formulation above. Note that this can

510 be done in either the time domain or the frequency domain; in the latter case, it should be noted
511 that our approach, through exploitation of small values of Womersley number, is considerably
512 simpler than the method of Flores et al. (2016). The approach can of course be applied to networks
513 of arbitrary complexity as long as the assumptions are valid in every vessel, although for very large
514 networks it would be more likely that alternative methods (such as homogenisation techniques)
515 would be applied, see for example the approach proposed by El-Bouri and Payne (2015).

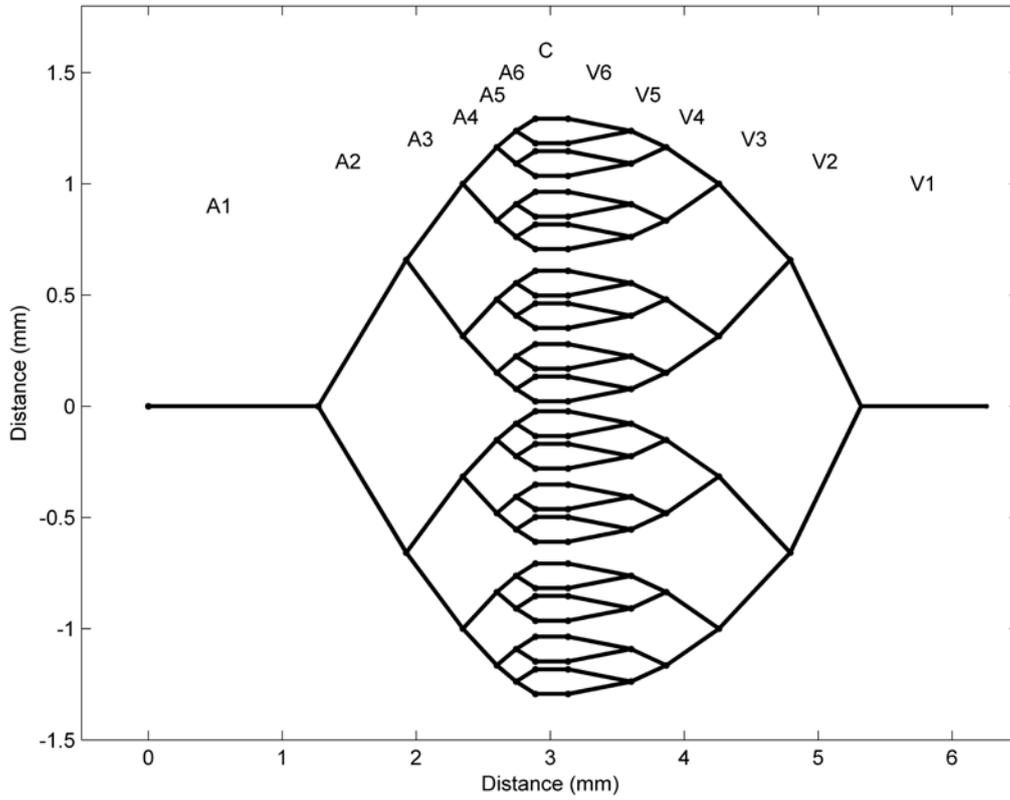
516 **3 Numerical simulations**

517 Having completed this analysis, we now consider the results in the context of previous models. In
518 particular we directly consider those models that model dynamic changes in the flow field. These
519 models, Boas et al. (2008), Reichold et al. (2009), Gagnon et al. (2015) and Payne and Lucas (2017),
520 are actually very similar in their approach, using a non-linear compliance model coupled with the
521 Poiseuille equation that uses an empirical model for viscosity based on vessel diameter and
522 haematocrit (which is taken to vary with vessel diameter). Although we have assumed a constant
523 compliance in our analysis here, we have shown that the assumption of quasi steady state (inherent
524 in all of the models listed above) is a valid one over all of the length scales that occur within the
525 cerebral vasculature.

526 However, we have shown in our analysis how to model the dynamic relationship between flow and
527 pressure in individual vessels and this has not been considered by the models listed above, where
528 only the leading order (Poiseuille) term is considered. Although the result given in Equation 55 is
529 more complicated, the dynamic term is not negligible in time-varying flow fields. We will illustrate
530 the effect that this can have in the simulations that we present below.

531 We consider the very simple bifurcating network shown in Figure 2 below, where we take the vessel
532 properties from the model proposed by Payne and Lucas (2017), as given in Table 2. We use this
533 network model as it is very similar to that proposed by Boas et al. (2008), where different modelling

534 assumptions were applied, as we will discuss below. It thus provides a simple means of comparison
 535 of the dynamic behaviour of the model.



536

537

Figure 2 Bifurcating network used in model simulations

Branch	Number of vessels	Diameter	Length	Wall thickness	Velocity	Viscosity	Pressure drop	Saturation
		μm	μm	μm	mm/s	mPa.s	mmHg	%
A1	1	23.97	1267.6	4.84	8.2	1.59	6.93	94
A2	2	19.17	930.3	4.25	6.41	1.50	5.87	93
A3	4	15.28	543.6	3.81	5.05	1.42	4.02	92
A4	8	12.08	302.3	3.49	4.03	1.34	2.70	89
A5	16	9.46	161.2	3.27	3.29	1.28	1.82	84

A6	32	7.32	154.7	3.14	2.75	1.23	2.35	76.5
C	64	8	243.9	0.309	2.30	1.24	2.62	66.5
V6	32	11.51	473.9	1.15	1.11	1.33	1.27	61
V5	16	14.53	272.3	1.45	1.40	1.40	0.61	59.75
V4	8	17.79	426.6	1.78	1.86	1.48	0.89	58.75
V3	4	21.45	632.5	2.15	2.56	1.55	1.31	58.25
V2	2	25.70	844.2	2.57	3.57	1.62	1.78	57.75
V1	1	30.77	936.3	3.08	4.97	1.70	2.01	57.25

538 **Table 2** Vascular parameters used in network model

539 For comparison, we plot the results obtained for the same network but using the flow and volume
540 model proposed by Boas et al. (2008) and used by other authors; the equations in this and in our
541 model are set out for comparison and for convenience of reference in Table 3. This approach
542 assumes that there is an instantaneous equilibrium between flow and pressure:

543
$$q_{ij} = \frac{1}{\mathcal{R}_{ij}} (p_i - p_j) \quad (72)$$

544 between nodes i and j , i.e. as Equation 55, but neglecting all dynamic terms. It then assumes that the
545 volume of each vessel, V_i , follows changes in pressure through a non-linear relationship of the form:

546
$$p_i - p_{ic} = kV_i^\beta \quad (73)$$

547 where k is a constant, set by baseline conditions, and β is a compliance parameter that is set to 2 by
548 Boas et al. (2008). The loop of equations is closed by conservation of volume:

549
$$\frac{dV_i}{dt} = q_{i,in} - q_{i,out} \quad (74)$$

550 These equations can easily be solved dynamically for the same dynamic inlet pressure and network
551 parameters given above.

	New approach	Previous approach
Pressure-flow relationship	$\begin{pmatrix} q_{in} \\ q_{out} \end{pmatrix} = \alpha_0 \begin{pmatrix} p_{in} \\ p_{out} \end{pmatrix} - \frac{R^2}{\nu} \alpha_2 \frac{d}{dt} \begin{pmatrix} p_{in} \\ p_{out} \end{pmatrix}$ <p>(Equation 55)</p>	$q_{ij} = \frac{1}{\mathcal{R}_{ij}} (p_i - p_j)$ <p>(Equation 72)</p>
Pressure-volume relationship	$V = \frac{C}{2} (p_{in} + p_{out})$ <p>(Equation 63)</p>	$p_i - p_{ic} = kV_i^\beta$ <p>(Equation 73)</p>
Flow-volume relationship	$\frac{dV}{dt} = q_{in} - q_{out}$ <p>(Equation 56)</p>	$\frac{dV_i}{dt} = q_{i,in} - q_{i,out}$ <p>(Equation 74)</p>
Nodal relationship	<p>Conservation of flow</p> <p>Matching of static pressure</p>	<p>Conservation of flow</p> <p>Matching of static pressure</p>

552 **Table 3** Summary of model equations in both approaches; for terminology, see original equations

553 We now illustrate our approach by considering the response to changes in inlet pressure. For
554 simplicity, we assume a reduction in inlet pressure from 60 mmHg to 48 mmHg (a drop of 20 %). In
555 order to give a smoothly varying inlet pressure, we assume a function of the form:

$$556 \quad p_{in} = P_a \left[1 + \left(\frac{k-1}{2} \right) \left(1 + \tanh \left(\frac{t-1}{0.1} \right) \right) \right] \quad (75)$$

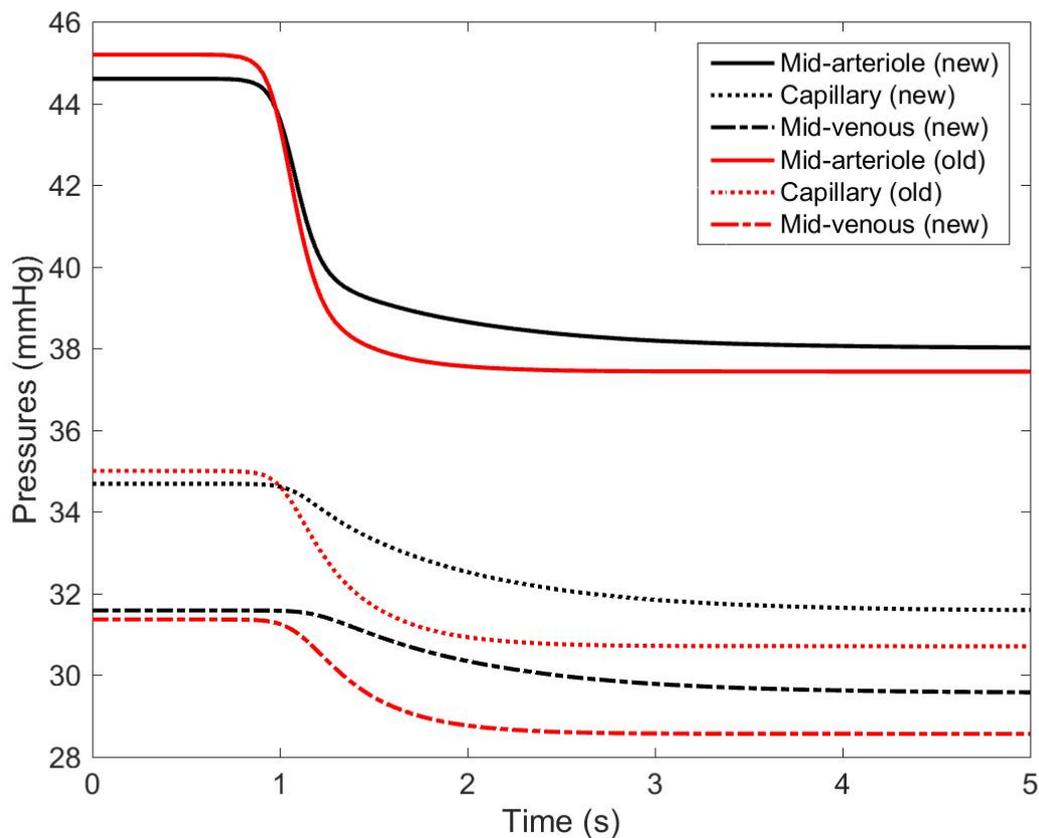
557 with k denoting the fractional value of baseline pressure to which the function tends, set here to 0.8
558 (i.e. a 20 % drop in driving pressure). This drop occurs at a time of 1 second (allowing the model to
559 settle before the change occurs) with a rapid rate of change. The resulting changes in nodal pressure
560 and vessel volume across all 13 generations are then calculated using both sets of model equations
561 set out in Table 4.

562 We first examine the changes in blood pressure within the network. Since our new approach is
563 based on nodal pressures and the previous approach on pressures in the middle of the vessel, we
564 interpolate the nodal pressures to plot the pressures half way along the vessels. We plot the
565 pressures in the third generation of the arteriolar bed, in the capillary bed, and in the fourth

566 generation of the venous bed for both models, as shown in Figure 3. We assume a value of 10 mmHg
567 for intracranial pressure and an exponent of 1 in Equation 73; we then calculate the value of k from
568 baseline conditions.

569 It is clear from Figure 3 that the changes in pressure propagate downstream from inlet to outlet,
570 with the largest and fastest changes occurring at the vessels closest to the inlet. Whilst the response
571 times to changes in inlet blood pressure in these vessels is of order only a couple of seconds, as
572 shown in Figure 3, we note that the response is not instantaneous, and care thus needs to be taken
573 in calculating the flow response to changes in inlet pressure since there is a delay in the propagation
574 of pressure changes through the network. Without considering the delay, there would be an
575 instantaneous response in all vessels.

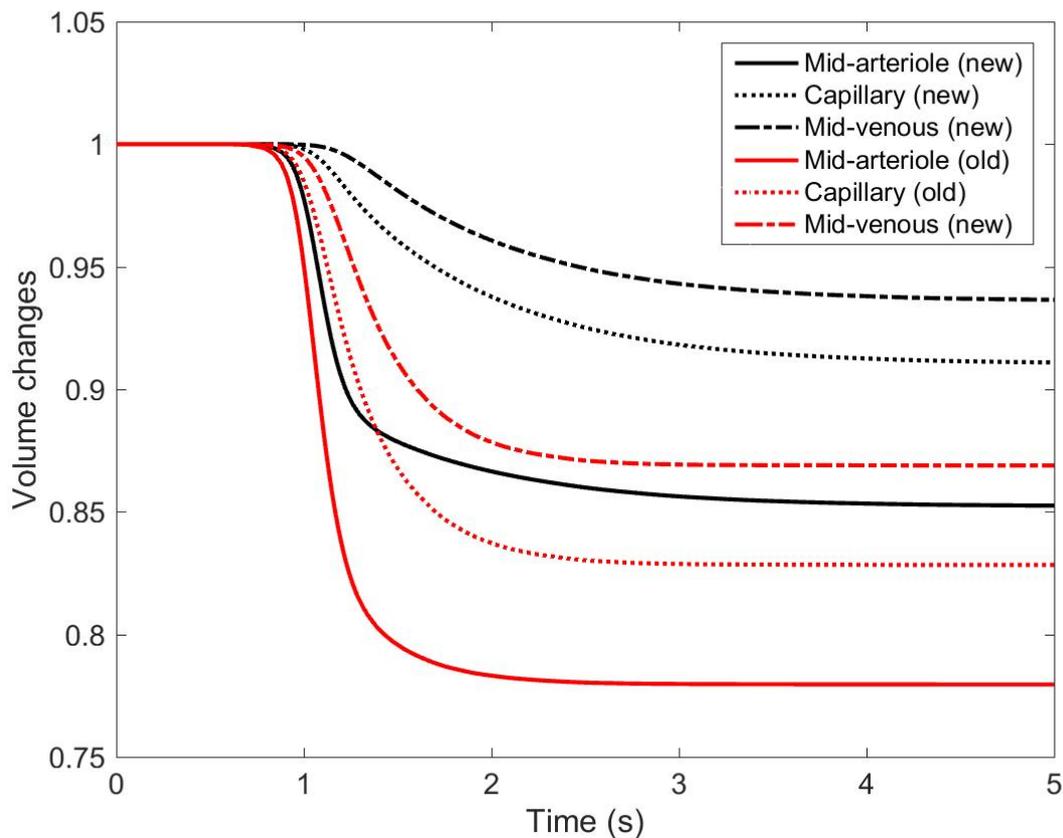
576 The previous model exhibits a much faster response throughout the vasculature; this is caused by
577 neglecting the second term in Equation 55. As a result, the speed of response is substantially
578 different; our model shows how the dynamic term in Equation 55 does play an important role in
579 setting the speed of response, even at this small length scale. Estimating the time constant of the
580 response yields values of 0.17, 0.76 and 1.15 seconds in our new model for the mid-arteriolar,
581 capillary and mid-venous vessels respectively, compared to 0.14, 0.34 and 0.47 seconds for the
582 previous model, showing how although the earlier vessels respond at a similar speed, the later
583 vessels respond much more slowly.



584

585 **Figure 3** Dynamic changes in blood pressures in bifurcating network in response to 20 % decrease in
 586 inlet blood pressure (for definitions of locations, see main text)

587 The results for volume, Figure 4, follow those for pressure, as would be expected from the analysis
 588 above and the justification of quasi steady state behaviour in response to changes in pressure. The
 589 later generations of the network thus respond much more slowly in response to changes in inlet
 590 blood pressure than would be assumed from the previous modelling approach. This difference is
 591 caused by the fact that previous approaches assumed a dynamically varying volume in response to
 592 instantaneous changes in pressure: our analysis shows rather that pressure responds dynamically to
 593 changes in inlet conditions with volume following these pressure changes quasi-statically (and hence
 594 with the same delay as the pressure changes).



595

596 **Figure 4** Dynamic changes in blood volumes in bifurcating network in bifurcating network in
 597 response to 20 % decrease in inlet blood pressure (for definitions of locations, see main text)

598 This is an important distinction and the fact that the changes in pressure and volume have now been
 599 shown to be slower than previously thought will significantly alter the dynamic behaviour of
 600 pressure and volume changes in models of the cerebral microvasculature. Note that the differences
 601 in absolute values of volumes between the two models, shown in Figure 4, are due to the slightly
 602 different models that are used for compliance in the two approaches; however this does not affect
 603 the main finding of this study. Experimental validation, through simultaneous measurements of
 604 blood flow and blood volume will be extremely valuable in validating the approach set out here and
 605 quantifying the importance of the dynamic term in Equation 55.

606 **4 Discussion**

607 In the previous section we have shown that the non-linear advection term can be neglected, when
608 considering both single vessels and the flow field as a continuum; derived a relationship between
609 inlet and outlet flows in single vessels and inlet and outlet pressures; derived the condition for a
610 quasi-steady-state approximation for blood volume; and then shown how single vessels can be
611 linked together and the flow field in a network solved as a matrix problem. For each of these
612 derivations there is a limit on the validity of the approximation: we thus consider these now in the
613 particular context of the cerebral vasculature. We will then also consider the limitations of the
614 approach that we have adopted. We should note that since we are basing many of the assumptions
615 on order of magnitude arguments, the precise values are often less important than the relative
616 magnitudes of different parameters.

617 We will assume throughout this section that blood has a density of 1040 kg/m^3 and a kinematic
618 viscosity of approximately $3 \text{ } \mu\text{Pa}\cdot\text{s}$ (we will consider the value of viscosity in more detail below) and
619 that the oscillation frequency is approximately 1 Hz (based on a typical heart rate of around 60 beats
620 per minute), see for example Caro et al. (2012). We can therefore quantify the magnitude of the
621 Womersley number immediately. This has magnitude less than one in vessels smaller than
622 approximately 1.4 mm in diameter. The first order model presented in Result 2 is thus only valid for
623 vessels of such diameter. Since the lower limit for imaging individual vessels is down to those with
624 diameters of approximately $0.8\text{-}0.9 \text{ mm}$, see for example Mut et al. (2014), this approach does thus
625 cover all of the generations of ‘unseen’ vessels and can therefore be applied to these vessels, i.e.
626 those of diameter less than approximately 1.4 mm .

627 We next consider the product ωT . As a first approximation, we assume the same elastic isotropic
628 model of the vessel wall as in Section 2.1; this then yields, see for example Chappell and Payne
629 (2016):

630
$$\omega T = 12 \left(\frac{\mu\omega}{E} \right) \left(\frac{L^2}{Rh} \right) \quad (76)$$

631 where the right hand side comprises non-dimensional groups, as shown in brackets, the latter based
632 on the geometry of the vessel and the former based on a mixture of properties. If we assume a value
633 of wall Young's modulus of 10^4 Pa, Caro et al. (2012), then this former term is approximately equal to
634 2×10^{-6} . The condition for the quasi-steady-state volume relationship then becomes
635 approximately $Rh/L^2 > 1.2 \times 10^{-7}$, which is satisfied by every vessel in the cerebral vasculature, since
636 the radius to length ratio is rarely less than 0.01 and the wall thickness to radius ratio is normally in
637 the range 0.1 to 0.5, see for example Payne (2007), Lucas (2012), Caro et al. (2012) and Payne (2017).
638 It is worth noting that this is in good agreement with recent studies into the neurovascular coupling
639 response, which have indicated a relatively small volume component to the short term response,
640 Hillman et al. (2007), Vazquez et al. (2010) and Drew et al. (2011). It also points away from the use of
641 the delayed compliance model, Kong et al. (2004) and Zheng and Mayhew (2009), since the time
642 constant has been shown here to be negligible in all vessels in the cerebral vasculature.

643 We next consider the ratio $\frac{E}{\rho U^2} \frac{h}{R}$, which needs to be much greater than 3/2 for advection to be
644 neglected. Since the ratio of wall thickness to radius, $\frac{h}{R}$, is typically in the range 0.1 to 0.5 (see above)
645 in any vessel, a lower bound for this can be taken to be 0.1: the ratio $\frac{E}{\rho U^2}$ needs to be much greater
646 than approximately 15. The flow velocity thus needs to be much less than $\sqrt{E/15\rho}$, which, for the
647 values of wall Young's modulus and blood density quoted above, is equivalent to being much less
648 than approximately 0.8 m/s. This is well above any flow velocity found in the cerebral vasculature
649 under normal conditions, Lucas (2012) and Payne (2017), and thus advection terms can be neglected
650 throughout the cerebral vasculature, although it should be noted that under certain conditions, for
651 example severe stenosis, flow velocities can rise substantially and that care would have to be taken
652 under such circumstances to re-evaluate this approximation.

653 Finally, we consider the product εRe_D , which should be below 100 for the difference between
654 matching of static and total pressures to be negligible. In the largest blood vessels in the brain, the

655 flow velocity is of order 0.5 m/s with diameters of order 5 mm, see for example Lucas (2012). Such
 656 values give a Reynolds number based on diameter of approximately 1000. Since the typical radius to
 657 length ratio values found in these large vessels are of order 0.1, Mut et al. (2014), the product εRe_D
 658 is thus of order 100 in the largest vessels in the brain. The difference between matched static and
 659 matched total pressure can thus be significant in these largest vessels; however, in the vessels below
 660 the imaging threshold of approximately 1 mm in diameter, Mut et al. (2014), this ratio will be below
 661 this limit, making the matching of static pressure a justifiable assumption in such vessels. Care simply
 662 needs to be taken when modelling the larger vessels, essentially those that can be imaged directly.
 663 In these vessels, the product εRe_D can be calculated for each vessel and the assumption of matched
 664 static pressure examined in each individual vessel.

665 We have thus explored how the four relationships derived earlier relate to individual blood vessels in
 666 the cerebral vasculature. It has been shown that advection can always be neglected in the equation
 667 governing blood flow and that blood volume can be assumed to be in quasi-steady state at all times;
 668 however, the first order approach for pressure and flow (arising from the perturbation series
 669 analysis) and the matching of static pressure should only be applied in vessels below approximately
 670 1 mm in diameter (using this as an approximate threshold for the distinction). Since this
 671 approximately corresponds to the imaging threshold, it is then possible to apply all four
 672 simplifications to models at this length scale. This does make the application of such models
 673 significantly easier. For simplicity we summarise these results in Table 4 below.

	Vessels of diameter < 1 mm	Vessel of diameter > 1 mm
Neglect advection	Yes	Yes
First order model	Yes	No
Blood volume quasi steady state	Yes	Yes
Match static pressure	Yes	Possibly

674 **Table 4** List of assumptions in vessels of different diameter

675 Note that whilst we have considered every vessel in each generation to respond in exactly the same
676 manner, due to the symmetry of the change that we have imposed (and for simplicity of
677 presentation), it would easily be possible to consider the response to localised changes in individual
678 vessels, as has been examined by other authors; although it should be noted that this model is at
679 present a purely passive one and that a model of the active response should be coupled with this
680 model in future to provide good agreement with experimental data, for example examining the
681 response to activation, as discussed in the Introduction.

682 It would be possible to characterise the overall behaviour of the network in terms of lumped values
683 of resistance and compliance, reducing the network to simpler form: characterising the response of
684 the network to changes in terms of time constants would be a valuable exercise, since this enables
685 the behaviour of the network to be considered as a whole, along the lines of the 6 second time
686 constant for oxygen transport in the same network found by Payne and Lucas (2017). This would
687 help to construct more detailed models of the larger vasculature, of which this network is only one
688 very small part. However, the approach set out in Table 3 under the restrictions set out in Table 4
689 can be used across the cerebral vasculature and it is suggested that these modelling equations,
690 validated by the analysis presented earlier, be used in this context in place of the other approaches
691 that have been used.

692 It is worth noting that alongside the model framework presented here that considers each vessel
693 individually, we also discussed earlier the use of a continuous approach to flow in the
694 microvasculature, based on the work of El-Bouri and Payne (2015) in providing a Darcy
695 approximation for the capillary flow field, as presented above, that has been coupled to a network
696 model in El-Bouri and Payne (2018), as shown in Figure 1d. This approach offers a complementary
697 method to the 'discrete' flow field presented here, since the two approaches can be coupled
698 together, dependent upon the length scale being considered and the size of the network that is

699 being studied, potentially reducing the computation time very significantly by exploiting the wide
700 range of length scales.

701 We do note that there are a number of limitations to the analysis above. We have assumed
702 axisymmetric vessels and flow fields, which is a reasonable assumption to these flows, although care
703 should be taken when considering vessels with any significant tortuosity. A more significant
704 assumption, however, is that we have assumed the fluid to be Newtonian, which does limit the
705 analysis. However, since the non-Newtonian effects will be greatest in the smaller vessels, which we
706 have found to be furthest away from the limits derived here, it thus seems reasonable to assume
707 that the non-Newtonian effects will have little impact on the results found here, although a more
708 rigorous analysis would be required to justify this more completely.

709 We have also neglected variations in haematocrit, which can have a significant impact on the flow
710 field throughout microvascular networks, Gould and Linninger (2015). The choice of model for
711 haematocrit distribution can also strongly influence the local flow patterns, although further
712 examination of the effects of this on the overall network behaviour is still needed. It would be
713 extremely interesting to examine the effects of the variability in haematocrit distribution on the
714 results that we have presented here.

715 In addition to this, future work will also involve extending the analysis to the transport of oxygen and
716 glucose between blood and tissue, using the approach set out in Payne and Lucas (2017), since
717 solving these equations is key to understanding the relationship between flow and metabolism. The
718 coupled nature of the equations means that this is a more difficult problem to investigate, although
719 considerable progress has been made by many of the studies listed in the Introduction. However, by
720 doing so, it will be possible to develop more rigorous models of both flow and metabolism that will
721 hopefully help to provide more insight into their behaviour in both normal and abnormal
722 physiological conditions.

723 This will also help to link to models of the BOLD response, providing a sounder theoretical
724 justification for the haemodynamic components of such models, in particular the lumped parameter
725 components, which often have to be assumed on a somewhat ad hoc basis, see for example Aquino
726 et al. (2014). Such multi-scale modelling approaches have a great deal to offer in terms of
727 understanding the relationship between the underlying physiology and experimental measurements
728 and provide a rich avenue for exploration in the future. They also offer the possibility of
729 experimental validation through the characterisation of models over different length scales, enabling
730 the assumptions used in the model proposed here to be more directly tested, using potentially a
731 very wide range of measurement modalities, including but not restricted to BOLD, MRI and PET.

732

733 **Appendix A**

734 A fundamental assumption when using homogenization is that the large-scale structure, in
 735 this case the capillary bed, is locally periodic. This allows the removal of secular terms in
 736 multi-dimensional problems without the need to solve higher order equations explicitly. It is
 737 of course possible to homogenize non-locally periodic structures, however finding the
 738 solvability condition to eliminate the secular terms becomes very difficult. Periodicity is thus
 739 regularly used in homogenization to simplify the removal of secular terms and is used here.

740 As $\varepsilon \ll 1$ the local and macro length scales are well-separated and can be defined as \mathbf{X} and
 741 $\mathbf{x} = \varepsilon\mathbf{X}$ respectively. Using the assumption of scale separation both \mathbf{x} and \mathbf{X} can be treated
 742 as independent variables and so

$$743 \quad \nabla = \nabla_{\mathbf{X}} + \varepsilon\nabla_{\mathbf{x}}, \quad \nabla^2 = \nabla_{\mathbf{X}}^2 + 2\varepsilon\nabla_{\mathbf{x}} \cdot \nabla_{\mathbf{X}} + \varepsilon^2\nabla_{\mathbf{x}}^2 \quad (\text{A. 1})$$

744 Using this to expand out Equation 17 gives:

$$745 \quad \varepsilon^2 Re_D [(\mathbf{u}_c \cdot \nabla_{\mathbf{X}})\mathbf{u}_c + \varepsilon(\mathbf{u}_c \cdot \nabla_{\mathbf{x}})\mathbf{u}_c] = -\nabla_{\mathbf{X}} p_c - \varepsilon\nabla_{\mathbf{x}} p_c + \varepsilon\nabla_{\mathbf{X}}^2 \mathbf{u}_c \\ + 2\varepsilon^2\nabla_{\mathbf{x}} \cdot \nabla_{\mathbf{X}} \mathbf{u}_c + \varepsilon^3\nabla_{\mathbf{x}}^2 \mathbf{u}_c \quad \text{in } \Omega_c \quad (\text{A. 2})$$

746 We also use non-dimensional forms of the continuity equation and the boundary conditions:

$$747 \quad \nabla_{\mathbf{X}} \cdot \mathbf{u}_c + \varepsilon\nabla_{\mathbf{x}} \cdot \mathbf{u}_c = 0 \quad \text{in } \Omega_c \quad (\text{A. 3})$$

$$748 \quad \mathbf{u}_c \cdot \mathbf{n} = 0 \quad \text{on } \Gamma_c \quad (\text{A. 4})$$

$$749 \quad \mathbf{u}_c \cdot \boldsymbol{\tau} = 0 \quad \text{on } \Gamma_c \quad (\text{A. 5})$$

750 where Ω_c denotes the blood space and Γ_c denotes the boundary between blood and tissue.
 751 We then apply the multiple scales expansion for velocity and pressure given in Equations 20
 752 and 21. In order to maintain periodicity each component of \mathbf{u} and p is assumed to be
 753 periodic in \mathbf{X} . The expansions of Equations 20 and 21 are substituted into Equations A.2-A.5
 754 and successive orders of ε equated to determine the leading order homogenized equations
 755 for capillary flow and pressure:

$$\begin{aligned}
& \varepsilon^2 \text{Rep} [((\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) \cdot \nabla_{\mathbf{X}}) (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) + \\
& \varepsilon ((\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) \cdot \nabla_{\mathbf{x}}) (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots)] = \\
756 \quad & -\nabla_{\mathbf{X}} (p_c^{(0)} + \varepsilon p_c^{(1)} + \dots) - \varepsilon \nabla_{\mathbf{x}} (p_c^{(0)} + \varepsilon p_c^{(1)} + \dots) + \varepsilon \nabla_{\mathbf{X}}^2 (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) \\
& + 2\varepsilon^2 \nabla_{\mathbf{x}} \cdot \nabla_{\mathbf{X}} (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) + \varepsilon^3 \nabla_{\mathbf{x}}^2 (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) \text{ in } \Omega_c \text{ (A. 6)}
\end{aligned}$$

$$757 \quad \nabla_{\mathbf{X}} \cdot (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) + \varepsilon \nabla_{\mathbf{x}} \cdot (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) = 0 \text{ in } \Omega_c \text{ (A. 7)}$$

$$758 \quad (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) \cdot \boldsymbol{\tau} = 0 \text{ (A. 8)}$$

$$759 \quad (\mathbf{u}_c^{(0)} + \varepsilon \mathbf{u}_c^{(1)} + \dots) \cdot \mathbf{n} = 0 \text{ (A. 9)}$$

760 Equating powers of $O(\varepsilon^0)$ in Equations A.6-A.9 gives:

$$761 \quad \nabla_{\mathbf{X}} p_c^{(0)} = 0 \text{ (A. 10)}$$

$$762 \quad \nabla_{\mathbf{X}} \cdot \mathbf{u}_c^{(0)} = 0 \text{ (A. 11)}$$

$$763 \quad \mathbf{u}_c^{(0)} \cdot \boldsymbol{\tau} = 0 \text{ and } \mathbf{u}_c^{(0)} \cdot \mathbf{n} = 0 \text{ on } \Gamma \text{ (A. 12)}$$

764 and equating powers of $O(\varepsilon^1)$:

$$765 \quad \nabla_{\mathbf{X}} p_c^{(1)} + \nabla_{\mathbf{x}} p_c^{(0)} = \nabla_{\mathbf{X}}^2 \mathbf{u}_c^{(0)} \text{ (A. 13)}$$

$$766 \quad \nabla_{\mathbf{X}} \cdot \mathbf{u}_c^{(1)} + \nabla_{\mathbf{x}} \cdot \mathbf{u}_c^{(0)} = 0 \text{ (A. 14)}$$

$$767 \quad \mathbf{u}_c^{(1)} \cdot \boldsymbol{\tau} = 0 \text{ and } \mathbf{u}_c^{(1)} \cdot \mathbf{n} = 0 \text{ on } \Gamma \text{ (A. 15)}$$

768 From Equation A.10 it is evident that $p_c^{(0)}$ is constant at the local-scale, hence $p_c^{(0)} = p_c^{(0)}(\mathbf{x})$.

769 In order to determine the leading order problem it is necessary to solve for $\mathbf{u}_c^{(0)}$ and $p_c^{(1)}$.

770 From Equation A.13 it can be seen that $\mathbf{u}_c^{(0)}$ and $p_c^{(1)}$ are both linear functions of $\nabla_{\mathbf{x}} p_c^{(0)}$ and

771 so solutions are proposed of the form:

$$772 \quad \mathbf{u}_c^{(0)} = -\mathbf{w}_c^j(\mathbf{X}) \frac{dp_c^{(0)}}{dx^j} \text{ (A. 16)}$$

$$773 \quad p_c^{(1)} = -P_c^j(\mathbf{X}) \frac{dp_c^{(0)}}{dx^j} + \bar{p}_c^{(1)} \text{ (A. 17)}$$

774 Einstein notation has been used here for clarity where j can take the values 1, 2, or 3 and
 775 refers to the Cartesian co-ordinate directions. The notation used is a simple substitution for
 776 what would otherwise be a dot product of the two j components. $\mathbf{w}_c^j(\mathbf{X})$ and $P_c^j(\mathbf{X})$ account
 777 for the local variations in $\mathbf{u}_c^{(0)}$ and $p_c^{(1)}$ and are known as the cell variables. It is from these
 778 local variables that the homogenized macro-scale parameters of the blood flow in the
 779 capillary network can be determined. These variables are determined by inserting them into
 780 Equations A.10-A.12 to obtain the cell problem:

$$781 \quad \nabla_{\mathbf{x}} \cdot \mathbf{w}_c^j(\mathbf{X}) = 0 \quad \text{in } \Omega_c \quad (\text{A. 18})$$

$$782 \quad \nabla_{\mathbf{x}} P_c^j(\mathbf{X}) = \nabla_{\mathbf{x}}^2 \mathbf{w}_c^j(\mathbf{X}) + \mathbf{e}_j \quad \text{in } \Omega_c \quad (\text{A. 19})$$

$$783 \quad \mathbf{w}_c^j(\mathbf{X}) \cdot \boldsymbol{\tau} = 0 \quad \text{and} \quad \mathbf{w}_c^j(\mathbf{X}) \cdot \mathbf{n} = 0 \quad \text{on } \Gamma \quad (\text{A. 20})$$

784 where \mathbf{e}_j is the unit vector in the j -direction. This is the local periodic cell problem which
 785 must be solved numerically in order, as shall be seen, to derive the parameters for the
 786 macro-scale problem. Note that Equation A.19 is a forced Stokes flow problem. From this is
 787 derived the Poiseuille equation (making assumptions on the radial and swirl components of
 788 the velocity). Therefore, despite having left in the convective acceleration term in the
 789 original equations, to leading order the cell problem is Stokes flow.

790 From Equations A.19-A.20 it can be seen that the cell problem is underdetermined and
 791 hence the local pressure term P_c^j is only defined up to a constant value. A uniqueness
 792 condition is thus imposed which states that the volume average of the local pressure is zero:

$$793 \quad \langle P_c^j \rangle_c = \frac{1}{|\Omega|} \int_{\Omega_c} P_c^j dV = 0 \quad (\text{A. 21})$$

794 Taking a volume average over $\mathbf{u}_c^{(0)}$, Equation A.16 results in:

$$795 \quad \langle \mathbf{u}_c^{(0)} \rangle_{\Omega_c} = -\mathbf{K} \nabla_{\mathbf{x}} p_c^{(0)} \quad (\text{A. 22})$$

796 where

$$797 \quad K_{ij} = \frac{1}{|\Omega|} \int_{\Omega_c} w_{ci}^j dV \quad (\text{A. 23})$$

798 This is Darcy's Law with \mathbf{K} defining the permeability tensor. Therefore, to leading order, the
799 homogenization of the incompressible, steady state Navier-Stokes equations gives Darcy's
800 Law. The permeability tensor \mathbf{K} encapsulates the geometry of the problem and how the
801 geometry affects the flow for given pressure gradients. It is an averaged coefficient tensor,
802 calculated by solving the micro cell problem, and is the volume average of the velocities in
803 the cell problem.

804

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